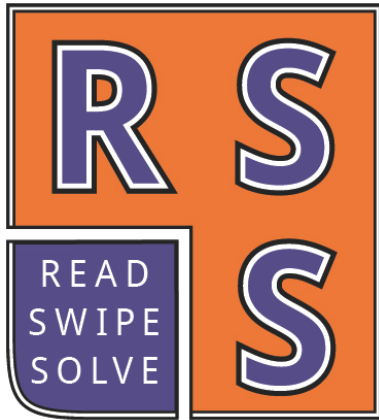
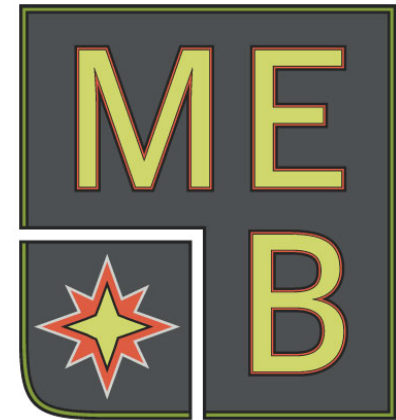


A 21st Century Textbook for Material and Energy Balances



Matthew Liberatore



COLORADOSCHOOL**OF MINES**
engineering the way

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Disclaimer: I own Read Swipe
Solve LLC and will financially
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Start With A Literature Review



“The students receiving the multimedia learning modules performed significantly better on both tests than the students experiencing the text-based presentations” T. Stelzer, et al., Am. J. Phys. 2009, 77, 184–190.

“Students also reported limitations of the textbook, contrasting it to the diversity of resources available via the Internet” C. S. Lee, et al., J. Eng. Ed. 2013, 102, 269–288.

“Participants with pre-lesson quiz scores in the lower-quartile improved 64% more (p -value < 0.001) with the interactive web-native content than with the static web content.” Edgcomb & Vahid, ASEE Conf. Proc. 2014. (zyante.com)

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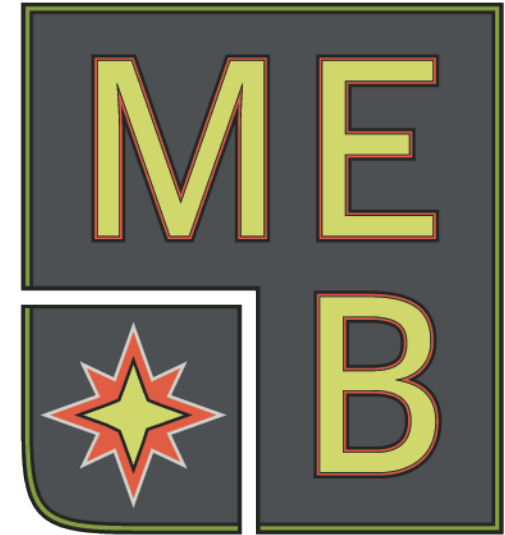
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Pen



Printing Press



Textbooks



Adobe

PDF & ePubublishing

Why Software Trumps 'Print'



Type of Textbook	Cost	Interactivity	Updates
Fundamentals of Material and Energy Balances	\$29.99 for web, iOS, Android	Yes	Frequent
Traditional Textbook	\$71.50 for Kindle	No	Once per decade

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MEB = The comprehension course



The 1st chemical engineering course

A gateway to the rest of the curriculum

Concepts covered:

- Mass/mole/atom balances

- Reacting systems

- Vapor-liquid equilibrium

- Energy balances

- Transient systems

Building from the bottom up



Goal: Develop problem solving skills and conceptual understanding

How:

Quick hitting concepts

Scaffolded, tiered examples

Interactivity and decision making

Bring Active Learning To The Textbook

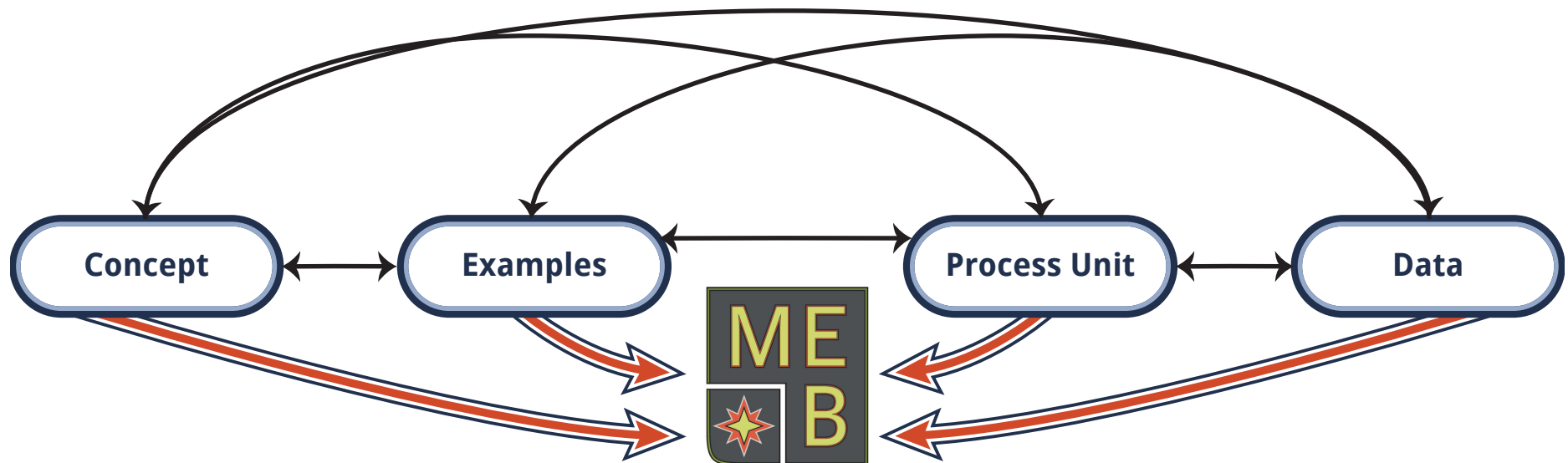
Scaffolded Tool for Active Reading[©]



Minimum Text

Non linear

Interactive Feedback



Quick Hitting Concepts



Fundamentals of Material and Energy Balances

Concept: Raoult's law

Raoult's law practice

Concept: Bubble and dew point

Constructing a two component pressure-composition (Pxy) diagram

Constructing a two component temperature-composition (Txy) diagram

Flash separation

Example[+]: Closed vessel with BT

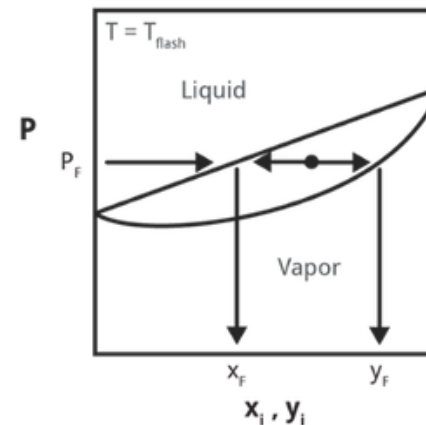
Closed vessel with BT - concept question

Closed vessel with BT - answers only

< Bubble and dew point

Flash separation

Flash is another type of vapor-liquid equilibrium. In this case, a fluid of known composition is placed at a set temperature and pressure. The temperature and pressure are selected so at equilibrium both vapor and liquid phases are present. Generally, one of the product phases (liquid or vapor) contains a large fraction of one of the species from the initial mixture.



6-5

Figure 6.5 Pxy diagram showing flash separation

Flashcards = interactive definitions



Properties of water

Water is a very well studied substance, and a wealth of tabulated water properties are available. Reading the "steam tables" is an important skill to determining properties from density to enthalpy for liquid and vapor water. Some general vocabulary and simple phase diagrams are introduced and then some rules of thumb on determining the phase and properties from given information concludes this concept. While steam tables are provided in the [Appendix](#), the concepts for the properties of water translate to most single species.

Six basic terms are defined here. The terms bubble point and dew point are covered in [Chapter 6](#).

PHASE	PHASE BOUNDARY	SATURATED
SATURATION T	SATURATION P	PHASE DIAGRAM

Next, the basic phases of water and pure substances are defined.

☰ Concept: Properties of water

Notes 0

ADD NOTE +

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Flashcards = interactive definitions



Properties of water

Water is a very well studied substance, and a wealth of tabulated water properties are available. Reading the "steam tables" is an important skill to determining properties from density to enthalpy for liquid and vapor water. Some general vocabulary and simple phase diagrams are introduced and then some rules of thumb on determining the phase and properties from given information concludes this concept. While steam tables are provided in the [Appendix](#), the concepts for the properties of water translate to most single species.

Six basic terms are defined here. The terms bubble point and dew point are covered in [Chapter 6](#).

Different forms that a pure substance can exist. Solid, liquid, and gas are the most common	PHASE BOUNDARY	Two phases existing in equilibrium
SATURATION T	P where vaporization starts at a given T	PHASE DIAGRAM

Next, the basic phases of water and pure substances are defined.

☰ Concept: Properties of water

Notes 0

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Choose Your Example/Adventure



C6 flash

A liquid mixture containing 79 mol% cyclohexane and the balance n-pentane enters a flash tank. The tank is maintained at 98°C and 29 psia. The flow rate of the entering stream is 96 mol/min.

Part a. Draw and label a process flow diagram.

Part b. Find the molar flow rates (mol/min) and mole fractions of the exiting stream(s).

Concept question. The entering flow rate increases by 17%, the composition of the pentane in the exiting liquid stream will increase, decrease or stay the same.

Jump to different levels using links:

[Problem statement](#)[Numerical answers](#)[Diagram only](#)[Equations only](#)[Full Solution](#)[Concept question](#)

Example: Numerical Answers



Numerical answers

$$x_{2,C} = \boxed{0.914}$$

$$y_{3,C} = \boxed{0.757}$$

$$x_{2,P} = \boxed{0.086}$$

$$y_{3,P} = \boxed{0.243}$$

$$\dot{n}_2 = \boxed{20.4 \frac{\text{mol}}{\text{min}}}$$

$$\dot{n}_3 = \boxed{75.6 \frac{\text{mol}}{\text{min}}}$$

Example: Diagram



Diagram



Figure 6.6a  C6 flash PFD

Example: Equations



Equations

$$\dot{n}_1 = \dot{n}_2 + \dot{n}_3$$

$$y_{1,C} \cdot \dot{n}_1 = x_{2,C} \cdot \dot{n}_2 + y_{3,C} \cdot \dot{n}_3$$

$$y_{3,C} \cdot P = x_{2,C} \cdot P_C^{\text{sat}}$$

$$y_{3,P} \cdot P = x_{2,P} \cdot P_P^{\text{sat}}$$

$$1 = x_{2,P} + x_{2,C}$$

$$1 = y_{3,P} + y_{3,C}$$

Example: Full Solution



Step 2 Stream 1

Step 3 Only 1 system to write balances.

Steps 4, 5, 6 Mole balances

Overall: $\dot{n}_1 = \dot{n}_2 + \dot{n}_3$

Component C: $y_{1,C} \cdot \dot{n}_1 = x_{2,C} \cdot \dot{n}_2 + y_{3,C} \cdot \dot{n}_3$

Step 7 Two Raoult's laws, Antoine equation, and two sum of mole fractions.

Raoult's Law C: $y_{3,C} \cdot P = x_{2,C} \cdot P_C^{\text{sat}}$

Raoult's Law P: $y_{3,P} \cdot P = x_{2,P} \cdot P_P^{\text{sat}}$

Sum mole fractions: $1 = x_{2,P} + x_{2,C}$

Sum mole fractions: $1 = y_{3,P} + y_{3,C}$

Antoine equation: $\log_{10} P^{\text{sat}} = A - \frac{B}{T + C}$

Steps 8, 9, 10, 11 6 unknowns: 2 balances, 2 Raoult's laws, 2 sum mole fractions. Solve.

Use given T and Antoine equation to find P^{sat} values.

$P_C^{\text{sat}}(T = 98^\circ\text{C}) = 1242 \text{ mmHg} = 165600 \text{ Pa}$

$P_P^{\text{sat}}(T = 98^\circ\text{C}) = 4224 \text{ mmHg} = 563100 \text{ Pa}$

Many ways to solve this system of equations. One way is:

Plug sum mole fractions in Raoult's Law for P. Solve Raoult's law C for $y_{3,C}$ and

plug $y_{3,C}$ into Raoult's Law P. Solve for $x_{2,C}$.

$$y_{3,C} = \frac{x_{2,C} \cdot P_C^{\text{sat}}}{P} \text{ and } (1 - y_{3,C}) \cdot P = (1 - x_{2,C}) \cdot P_P^{\text{sat}} \rightarrow$$

$$x_{2,C} = \frac{P - P_P^{\text{sat}}}{P_C^{\text{sat}} - P_P^{\text{sat}}} \rightarrow x_{2,C} = \boxed{0.914}$$

$$y_{3,C} = \frac{x_{2,C} \cdot P_C^{\text{sat}}}{P} \rightarrow y_{3,C} = \boxed{0.757} \text{ and } x_{2,P} = \boxed{0.086} \quad y_{3,P} = \boxed{0.243}$$

Plug overall balance into component balance to find flow rates.

$$y_{1,C} \cdot \dot{n}_1 = x_{2,C} \cdot \dot{n}_2 + y_{3,C} \cdot (\dot{n}_1 - \dot{n}_2) \rightarrow \dot{n}_2 = \boxed{20.4 \frac{\text{mol}}{\text{min}}} \text{ and } \dot{n}_3 = \boxed{75.6 \frac{\text{mol}}{\text{min}}}$$

Step 12 Check using component P balance or any atom balance.

12 steps problem solving method

Example: Full Solution



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Step 3 Only 1 system to write balances.

Steps 4, 5, 6 Mole balances

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$$y_{3,C} = \frac{x_{2,C} \cdot P_C^{\text{sat}}}{P} \text{ and } (1 - y_{3,C}) \cdot P = (1 - x_{2,C}) \cdot P_P^{\text{sat}} \rightarrow$$

$$x_{2,C} = \frac{P - P_P^{\text{sat}}}{P_C^{\text{sat}} - P_P^{\text{sat}}} \rightarrow x_{2,C} = \boxed{0.914}$$

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12 steps problem solving method

Example: Concept Question



Question 1

A liquid mixture containing 79 mol% cyclohexane and the balance n-pentane enters a flash tank. The tank is maintained at 98°C and 29 psia. The flow rate of the entering stream is 96 mol/min.

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Concept question. The entering flow rate increases by 17%, the composition of the pentane in the exiting liquid stream will:

Increase

Decrease

Stays the same

Need help with this one? [Get a hint](#) or [show answer](#).

CHECK ANSWER

② C6 flash - concept question



Scoreboard

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0%
Complete

■ Correct	0
■ Wrong	0
■ Unanswered	1

Total 1

Notes 0

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Example: Concept Question



Question 1

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Increase

Decrease

Stays the same

How does Raoult's law vary with flow rate?

Need help with this one? [Get a hint](#) or [show answer](#).

CHECK ANSWER

? C6 flash - concept question



Scoreboard

Start Over

0%
Complete

Correct	0
Wrong	0
Unanswered	1
Total	1

Notes 0

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Example: Concept Question



Question 1

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Concept question. The entering flow rate increases by 17%, the composition of the pentane in the exiting liquid stream will:

Increase

Decrease

Stays the same



That's correct!

The flow rate does not change the compositions exiting the tank. Raoult's law is independent of flow rate.

Need help with this one? [Get a hint.](#)

DONE

? C6 flash - concept question



Scoreboard

[Start Over](#)



Correct	1
Wrong	0
Unanswered	0

Total 1

Notes 0

[ADD NOTE +](#)

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Process Unit



Flash tank

Flash separation is a simple process unit where T , P are altered to create separation of one or more components. The exiting vapor and liquid streams are in equilibrium providing one extra equation for each component in equilibrium. The process may be called flash evaporation and the equipment is commonly known as a flash drum. Additional information on flash can be found [elsewhere](#).



6-13

Figure 6-13  Flash tank.

Process Unit: External Resources



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Flash evaporation

From Wikipedia, the free encyclopedia

Flash (or partial) evaporation is the partial vapor that occurs when a [saturated liquid](#) stream undergoes a reduction in pressure by passing through a [throttling valve](#) or other throttling device. This process is one of the simplest [unit operations](#). If the throttling valve or device is located at the entry into a [pressure vessel](#) so that the flash evaporation occurs within the vessel, then the vessel is often referred to as a [flash drum](#).^{[1][2]}

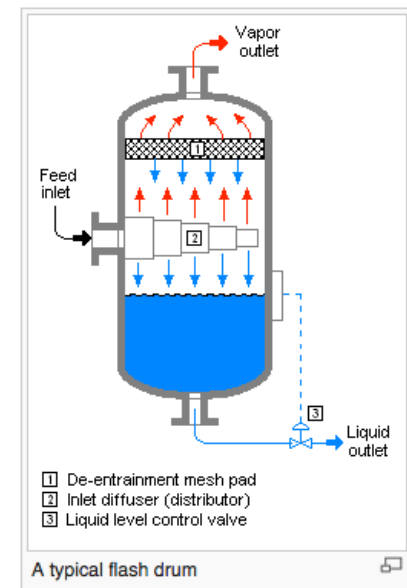
If the saturated liquid is a single-component liquid (for example, liquid [propane](#) or liquid [ammonia](#)), a part of the liquid immediately "flashes" into vapor. Both the vapor and the residual liquid are cooled to the [saturation temperature](#) of the liquid at the reduced pressure. This is often referred to as "auto-refrigeration" and is the basis of most conventional [vapor compression refrigeration](#) systems.

If the saturated liquid is a multi-component liquid (for example, a mixture of [propane](#), [isobutane](#) and normal [butane](#)), the flashed vapor is richer in the more [volatile](#) components than is the remaining liquid.

Uncontrolled flash evaporation can result in a boiling liquid expanding vapor explosion ([BLEVE](#)).

Contents [\[hide\]](#)

- 1 Flash evaporation of a single-component liquid
- 2 Equilibrium flash of a multi-component liquid
- 3 Contrast with spray drying
- 4 Natural flash evaporation
- 5 See also
- 6 References
- 7 External links





Antoine equation constants for determining vapor pressure

Vapor Pressure (or Saturation Pressure) is discussed in [Chapter 5](#). The Antoine equation is a very common way to determine vapor pressure as a function of temperature. Three constants are needed to calculate vapor pressures from the Antoine equations. These constants are tabulated here for many common compounds.

$$\log_{10} P^{\text{sat}} = A - \frac{B}{T+C}$$

where A, B, C are tabulated here. P^{sat} has units of mmHg and T has units of °C. These tables can easily be copied to a spreadsheet for simplifying vapor pressure calculations.

Compound	Formula	A	B	C	Range (Low T)	Range (High T)
Chloroform	CHCl ₃	6.90328	1163.03	227.4	-30	150
Cyclohexane	C ₆ H ₁₂	6.84941	1206.001	223.148	19.9	81.6
Cyclohexanol	C ₆ H ₁₂ O	6.2553	912.866	109.126	93.7	160.7
n-Decane	n-C ₁₀ H ₂₂	6.95707	1503.568	194.738	94.5	175.1
1-Decene	C ₁₀ H ₂₀	6.95433	1497.527	197.056	86.8	171.6

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Most common complaints: Fix the typos, include all of the major course concepts, and data tables

Surveying the Students



Beta Test: Spring 2014 with 153 students

80% of class purchased FMEB

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Most common complaints types,
include all of the course concepts and
data tables

Completed Summer 2014

What's next? – Research Questions



Usage analytics: How well are students engaged, how long students reading the STAR format versus a traditional paper textbook, which levels of the questions are students using, which difficulty of scaffolded examples are the students using.

Can the 12 step problem solving technique be observed in a time restricted exam setting.

Can this technology be fully integrated with online homework (e.g., Sapling Learning) to provide instructors real time assessment of the students progress in problem solving and conceptual knowledge.

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Traditional Textbook	\$71.50 for Kindle	No	Once per decade

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